## Emergency Procedures for Utility or DCS Interruptions

## Overview

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| Introduction | This chapter describes what to do in the event of a major utility or DCS failure. |

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End of topic

#### Breathing Air System Shutdown

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| Introduction | This topic describes what to do if the breathing air system suddenly fails. |

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| Failure Notification | If an emergency condition develops that shuts down the compressor motor for any reason, a low pressure alarm sounds in the Monomer control room. Monomer will notify other users immediately. |

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| Immediate Action | When the compressor stops, there is sufficient air in the system to sustain two users for about 10 minutes. Get to a safe location and remove breathing air as soon as possible. |

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| During an Outage | While the breathing air system remains down, use Scott air paks or cylinder breathing air if breathing air is needed. Do NOT use instrument air or air from a portable compressor. Work that can wait for the breathing air system to be back on line should be stopped until the system is back up. |

End of topic

#### Site-wide Power Loss

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| Introduction | This procedure describes what to do in the event all electrical power is lost. |

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| What will Happen | In the event of a power failure, any batch in progress will essentially abort, and all automatic valves will fail to a safe state. The safe state for the majority of the valves is a closed position. Exceptions are valves that are air to close, including: ZnCl2 recycle valves (MWT pressure control), autoclave process water makeup valves, and autoclave jacket dump (pressure control) valves.  As liquid TFE temperature in the MWT and piping systems rise the pressure will increase and either activate the tanks rupture disk/relief valve or overpressure the vessel. Operators will vent the equipment to prevent these scenarios.  The PTFE liquid load header will be isolated by fail-closed automatic valves closing. Operators will vent the liquid header to the Mixed Gas Holder to prevent overpressure.  For an outage of any significant duration expect the MWT discharge line to the autoclave on-axis rupture disks to activate and vent the piping contents. |

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| Safety | 1. The breathing air system will be off-line during a site-wide power outage. 2. Wear breathing air (Scott air packs) if there is potential of being exposed to TFE vapors, for example, if you are in proximity to a TFE vent. Areas with a high potential for exposure to a TFE vent include inside the barricades (cells), the cell corridor, the blast area, and roof above the barricades. 3. Avoid entrance inside the barricades or the roof above the barricades while the Granular polykettles, FPD autoclaves, or Monomer Weigh Tanks are at high-operating pressure. 4. Avoid closing manual valves with potential to trap liquid TFE between the manual and closed automatics. Manuals should only be closed to prevent an on-going release. |

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| Environmental | When venting the monomer weigh tanks (MWT), only vent when necessary to minimize the amount of TFE vented to the atmosphere. |

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| Reference | For more information about activating the emergency shutdown system, see chapter 3, this section.  For information on venting the condensers and refined monomer storage tanks see Granular area emergency operating directions. |

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Site-wide Power Loss, Continued

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| Response | Follow these steps to respond to the power failure: |

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| **Step** | **Action** |
| 1 | Activate the TFE Polymers emergency shutdown system with one of the five push buttons (2569PB):   * Granular Polykettle DCS IER * Southeast corner of Fine Powder Dispersion DCS IER * East inside stairwell of Bldg. 162, on the 2nd floor * Turnaround area, southwest of Bldg. 162 * High Hazard Control Room (HHCR) northwest corner |
| 2 | Contact site ECO headquarters and activate shelter in place for possible fume release. |
| 3 | Vent the autoclave by opening the manual emergency vent valve in the autoclave 3rd level corridor. Vent the autoclave for 3-5 minutes before proceeding to the next step to make sure Monomer Weigh Tank (MWT) pressure is maintained greater than autoclave pressure. |
| 4 | Verify MWT emergency vent valves backup air-supply is within SOC, and then switch the air supply from plant air to emergency backup air. |
| 5 | Using the emergency vent valves, vent any MWT that was pressurized (>90 psig) before the power outage for 30 seconds and then close the vent valve. |
| 6 | Check in the field around all the monomer weigh tanks. Verify that the automatic emergency vent valves are closed. If any are open, close the manual valve in the vent line to stop the continuous vent. |
| 7 | Monitor the pressure in the monomer weigh tanks using the field gauges. When the pressure builds up to 110 psig, vent the monomer weigh tank down by opening the emergency vent valve. Keep the pressure in the tanks below 110 psig. |
| 8 | Monitor pressure in the trapped monomer weigh tanks liquid load line between the refined monomer storage tanks. There is a pressure gauge on the 3rd level of autoclave 7 below the vent valve, and on the header. Add a temporary gauge if one is not already installed and functioning. Vent the line to the Monomer mixed gas holder as necessary to maintain pressure less than 110 psig per the following steps:   * Contact Monomer to let them know a small amount of TFE will be vented back to the Mixed Gas Holder. Monomer should have the MGH relief valve vent stack blower running off diesel backup power. * Slowly open the auto valve on the 3rd level of autoclave 7 cell in the line connecting the liquid header to the MGH header until pressure is below 110 psig. |
| 9 | Continue to monitor the pressure in the monomer weigh tanks and liquid load line. Vent as needed to maintain pressure less than 110 psig. |
| 10 | When power comes back on, check temperatures and pressures of the TFE systems and establish brine flow as soon as possible to keep venting to a minimum.  Do not re-open automatic isolation valves until the integrity of all rupture disks is determined. |

End of topic

#### Electric Power Surge or Short-Term Loss

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| Introduction | This procedure describes what to do in the event of an electric power surge or short-term loss. For complete loss of power see “Site Wide Power Loss” in this operating direction. |

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| What will Happen | DCS systems may partially or completely fail. Batches will likely abort.  Autoclave and TFE system safety interlocks may activate, and trap liquid TFE in piping systems.  For an outage of any significant duration expect the MWT discharge on-axis rupture disks on any running autoclaves to activate and vent the piping contents. |

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| Safety | * Wear breathing air if there is potential of being exposed to TFE vapors, for example, if you are in proximity to a TFE vent. Areas with a high potential for exposure to a TFE vent include inside the barricades (cells), the cell corridor, the blast area, and roof above the barricades. * Avoid entrance inside the barricades or the roof above the barricades while the Granular polykettles, FPD autoclaves, or Monomer Weigh Tanks are at high-operating pressure. * Avoid closing manual valves with potential to trap liquid TFE between the manual and closed automatics. Manuals should only be closed to prevent an on-going release. |

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| Environmental | When venting the monomer weigh tanks only vent when necessary to minimize the amount of TFE vented to the atmosphere. |

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| Reference | For more information about activating the emergency shutdown system, see chapter 3, this section. |

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Electric Power Surge or Short-Term Loss, Continued

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| Response | Follow these steps to respond to a temporary loss of power: |

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| Step | Action |
| 1 | Attempt to reset MWT discharge on-axis rupture disk, and open the MWT fail-safe valve before these lines overpressure and activate the disk. Rupture disk that cannot be reset are likely activated. Verify disk activation in field, and proceed to section 33P4E2 for handling blown rupture disks. |
| 2 | Restart DCS systems per the last section of this operating direction. If DCS cannot be restarted, begin field monitoring of all MWT and TFE system pressures. |
| 3 | Verify with the Monomer area that cold brine is still being delivered to the TFE systems. If brine is loss, proceed to section in this operation direction for loss of -35 C cooling. |

End of topic

#### Plant (Instrument) Air Loss

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| Introduction | This procedure describes what to do in the event that plant air fails. |

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| What will Happen | If plant air is lost, any batch in progress will automatically abort, and all automatic valves will fail to a safe state. The safe state for the majority of the valves is a closed position. Exceptions are valves that are air to close, including: ZnCl2 recycle valves (MWT pressure control), Autoclave process water makeup valves, and Autoclave jacket dump (pressure control) valves.  Site-wide loss of plant air will very likely also result in loss of refrigeration (-35 C brine). As liquid TFE temperature in the MWT and piping systems rise the pressure will increase and either activate the tanks rupture disk/relief valve or overpressure the vessel. Operators will vent the equipment to prevent these scenarios.  The PTFE liquid load header will be isolated by fail-closed automatic valves closing. Operators will vent the liquid header to the Mixed Gas Holder to prevent overpressure.  For an outage of any significant duration expect the MWT discharge line to the autoclave on-axis rupture disks to activate and vent the piping contents. |

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| Safety | * Wear breathing air if there is potential of being exposed to TFE vapors, for example, if you are in proximity to a TFE vent. Areas with a high potential for exposure to a TFE vent include inside the barricades (cells), the cell corridor, the blast area, and roof above the barricades. * Avoid entrance inside the barricades or the roof above the barricades while the Granular polykettles, FPD autoclaves, or Monomer Weigh Tanks are at high-operating pressure. * Avoid closing manual valves with potential to trap liquid TFE between the manual and closed automatics. Manuals should only be closed to prevent an on-going release. |

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| Environmental | When venting the monomer weigh tanks only vent when necessary to minimize the amount of TFE vented to the atmosphere. |

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| Reference | For more information about activating the emergency shutdown system, see chapter 3, this section. |

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Plant (Instrument) Air Loss, Continued

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| Response | Follow these steps to respond to a loss of plant air: |

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| Step | Action |
| 1 | Activate the TFE Polymers emergency shutdown system with one of the five push buttons (2569PB):   * Granular DCS IER (instrument electrical room) * Southeast corner of Fine Powder Dispersion DCS IER * East inside stairwell of Bldg. 162, on the 2nd floor * Turnaround area, southwest of Bldg. 162 * High Hazard Control Room (HHCR) northwest corner |
| 2 | Contact site ECO headquarters and activate shelter in place for possible fume release. |
| 3 | Vent the autoclave by opening the manual emergency vent valve in the autoclave 3rd level corridor. Vent the autoclave for 3-5 minutes before proceeding to the next step to make sure Monomer Weigh Tank (MWT) pressure is maintained greater than autoclave pressure. |
| 4 | Verify MWT emergency vent valves backup air-supply is within SOC, and then switch the air supply from plant air to emergency backup air. |
| 5 | Monitor the pressure in the monomer weigh tanks at the DCS. If the pressure builds up to 110 psig, vent the tank down by opening the emergency vent valve. Keep the pressure in the tanks below 110 psig. |
| 6 | Check in the field around the monomer weigh tanks. Verify that any emergency vent valve supposed to be still closed is closed. If one of them is not closed, close the manual valve in the vent line to stop the continuous vent. |
| 7 | Monitor pressure in the trapped monomer weigh tanks liquid load line between the refined monomer storage tanks. There is a pressure gauge on the 3rd level of autoclave 7 below the vent valve, and on the header. Add a temporary gauge if one is not already installed and functioning. Vent the line to the Monomer mixed gas holder as necessary to maintain pressure less than 110 psig per the following steps:   * Contact Monomer to let them know a small amount of TFE will be vented back to the Mixed Gas Holder. * Slowly open the auto valve on the 3rd level of autoclave 7 cell in the line connecting the liquid header to the MGH header until pressure is below 110 psig. |
| 8 | Continue to monitor the pressure in the monomer weigh tanks and liquid load line. Vent as needed to maintain pressure less than 110 psig. |
| 9 | When instrument air comes back on, check temperatures and pressures of the TFE systems and establish brine flow as soon as possible to keep venting to a minimum.  Do not re-open automatic isolation valves until the integrity of all rupture disks is determined. |

End of topic

#### Process Water Loss

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| Introduction | This procedure describes what to do in the event that plant process cooling water is lost. |

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| What will Happen | If process water is lost, any batch in progress will automatically abort.  Process water provides cooling for the autoclave reaction. Failure of the batch to abort under these conditions could result in overpressure of the autoclave. |

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| Safety | No special safety precautions. |

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| Environmental | No special environmental precautions. |

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| Reference | For more information about activating the emergency vent valves, see chapter 3, this section. |

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| Response | Follow these steps to respond to a loss of process water: |

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| Step | Action |
| 1 | Verify that batch has aborted, and that TFE feed has shutoff. If the batch has not aborted, activate the autoclave emergency shutdown button. |

End of topic

#### Steam, Nitrogen, or Cell Ventilation Loss

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| Introduction | This procedure describes what to do in the event that plant steam, nitrogen, or cell ventilation is lost. |

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| What will Happen | There are no immediate safety consequences for loss of the above listed services. Steam is used to heat and deareate water; and to maintain autoclave temperature when TFE is added without start of reaction. Steam is also used for vacuum. Nitrogen is used for sweeping the autoclave. Cell ventilation is required to prevent accumulation of chemical vapors. |

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| Safety | No special safety precautions for steam or nitrogen loss.  Monitor IR analyzer results in the cells if ventilation is offline. Use breathing air to enter the cell if TFE levels are elevated. |

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| Environmental | No special environmental precautions. |

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| Reference | None |

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| Response | Follow these steps to respond to a loss of steam: |

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| Step | Action |
| 1 | Any autoclave batch not yet in reaction should be aborted. |
| 2 | Any autoclave batch in reaction or venting should be completed. |
| 3 | Wait until service is restored before starting another batch. |

End of topic

#### Refrigeration (-35 C Brine) Loss of Flow

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| Introduction | This procedure describes what to do in the event that refrigeration (-35 C brine) from Monomer fails and there is no/low flow of cold brine. |

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| What will Happen | As liquid TFE temperature in the MWT and piping systems rise the pressure will increase. Trapping any liquid TFE without cooling will result in either activation of a rupture disk/relief or overpressure of the vessel or piping system. Do not isolate liquid with automatic or manual valves under this scenario unless necessary to prevent loss of containment (activated rupture disk).  Operators will vent equipment either back to Monomer, if Monomer can accept vents, or to the atmosphere. |

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| Safety | Wear breathing air if there is potential of being exposed to TFE vapors, for example, if you are in proximity to a TFE vent. Areas with a high potential for exposure to a TFE vent include inside the barricades (cells), the cell corridor, the blast area, and roof above the barricades.  Avoid entrance inside the barricades or the roof above the barricades while the autoclave, FPD autoclaves, or Monomer Weigh Tanks are at high-operating pressure. |

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| Environmental | When venting the monomer weigh tanks, only vent when necessary to minimize the amount of TFE vented to the atmosphere. |

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| Reference | None |

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Refrigeration (-35 C Brine) Loss of Flow, Continued

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| Response | Follow these steps to respond to a loss of refrigeration: |

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| Step | Action |
| 1 | Do not immediately activate the TFE Polymers emergency shutdown or individual TFE system emergency shutdown systems. This will trap liquid TFE in now-unrefrigerated piping and vessels and result in more releases and venting. |
| 2 | Complete any autoclave batch for which the autoclave has already been pressurized. Continued removal of TFE from the monomer weigh tank will reduce the need for both TFE system and autoclave venting. |
| 3 | Stop loading monomer weigh tanks. Under these conditions the Monomer mixed gas holder capacity will be severely limited. |
| 4 | Depressure (to less than 100 psig) any monomer weigh tank not feeding a autoclave by one of the two following methods:   * (preferred) – Depressure the monomer weigh tank per standard procedures for ZnCl2 drainback. NOTE: Monitor mixed gas holder level and/or ZnCl2 vent header pressure closely to avoid blowing the header rupture disk. * (or) – Vent the tank down by opening the emergency vent valve. |
| 5 | For any monomer weigh tank not feeding an autoclave verify the ZnCl2 drain valve is closed and the failsafe valve to the autoclave is open. Open the monomer weigh tank balance line valves to allow the monomer weigh tank to ride on refined monomer storage tank pressure. |
| 6 | Granular will monitor the pressure in the refined monomer storage tanks at the DCS. If the pressure builds up to 110 psig, vent the tank down by opening the emergency vent valve on one or more of the RMST. Keep the pressure in the tanks below 110 psig. |
| 7 | Vent down any monomer weigh tanks for completed or aborted autoclave batches per step 3 through 5 above. |
| 8 | Continue to monitor the pressures in the tanks and vent as needed. |
| 9 | If a monomer weight tank pressure cannot be maintained below 110 psig by venting the refined monomer storage tanks, close the liquid load and balance line valves. Vent the monomer weight tank with the emergency vent valve. |

End of topic

#### Refrigeration (-35 C Brine) Loss of Temperature Control

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| Introduction | This procedure describes what to do in the event that refrigeration (-35 C brine) from Monomer fails but brine continues to flow to the process. |

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| What will Happen | With no cooling from the Monomer refrigeration units the brine will be quickly heated by the transfer pumps. This will result in “hot” brine being delivered to the MWT and piping systems. The liquid TFE temperature in the RMSTs, Condensers, MWT and piping systems will rapidly increase resulting in either activation of a rupture disk/relief or overpressure of the vessel or piping system. This event will happen much faster than a loss of brine flow. Do not isolate liquid TFE with automatic or manual valves under this scenario unless necessary to prevent loss of containment (activated rupture disk).  Operators will isolate the brine supply to the area first, then vent equipment either back to Monomer, if Monomer can accept vents, or to the atmosphere. |

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| Safety | Wear breathing air if there is potential of being exposed to TFE vapors, for example, if you are in proximity to a TFE vent. Areas with a high potential for exposure to a TFE vent include inside the barricades (cells), the cell corridor, the blast area, and roof above the barricades.  Avoid entrance inside the barricades or the roof above the barricades while the autoclave, FPD autoclaves, or Monomer Weigh Tanks are at high-operating pressure.  Do not shut both the brine supply and return, this will result in overpressure of the brine header. |

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| Environmental | When venting the monomer weigh tanks, only vent when necessary to minimize the amount of TFE vented to the atmosphere. |

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| Reference | None |

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Refrigeration (-35 C Brine) Loss of Temp. Control, Continued

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| Response | Follow these steps to respond to a loss of refrigeration when brine flow continues: |

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| Step | Action |
| 1 | Close area brine supplies to both the B162 vessel jackets, tracing and all three TFE Condensers. In this kind of event stopping brine flow will extend the time before TFE venting is required.   * B162 brine supply is located to the west of the base of the RMSTs, just outside the Monomer stairwell door. The valves are labeled with a placard. * Condenser brine supply has an isolation valve on the blue grating north of the still house. The supply and returns are labeled with a green placard.   DO NOT shut both the supply and the return this will result in overpressure of the brine header. |
| 2 | Do not immediately activate the TFE Polymers emergency shutdown or individual TFE system emergency shutdown systems. This will trap liquid TFE in now-unrefrigerated piping and vessels and result in more releases and venting. |
| 3 | Complete any autoclave batch for which the autoclave has already been pressurized. Continued removal of TFE from the monomer weigh tank will reduce the need for both TFE system and autoclave venting. |
| 4 | Stop loading monomer weigh tanks. Under these conditions the Monomer mixed gas holder capacity will be severely limited. |
| 5 | Depressure (to less than 100 psig) any monomer weigh tank not feeding an autoclave by one of the two following methods:   * (preferred) – Depressure the monomer weigh tank per standard procedures for ZnCl2 drainback. NOTE: Monitor mixed gas holder level and/or ZnCl2 vent header pressure closely to avoid blowing the header rupture disk. * (or) – Vent the tank down by opening the emergency vent valve. |
| 6 | For any monomer weigh tank not feeding an autoclave verify the ZnCl2 drain valve is closed and the failsafe valve to the autoclave is open. Open the monomer weigh tank balance line valves to allow the monomer weigh tank to ride on refined monomer storage tank pressure. |
| 7 | Monitor the pressure in the refined monomer storage tanks at the DCS. If the pressure builds up to 110 psig, contact Granular to vent the tank down by opening the emergency vent valve on one or more of the RMST. Keep the pressure in the tanks below 110 psig. |
| 8 | Vent down any monomer weigh tanks for completed or aborted autoclave batches per step 3 through 5 above. |
| 9 | Continue to monitor the pressures in the tanks and vent as needed. |
| 10 | If a monomer weight tank pressure cannot be maintained below 110 psig by venting the refined monomer storage tanks, close the liquid load and balance line valves. Vent the monomer weight tank with the emergency vent valve. |

End of topic

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#### Responding to a DCS Failure

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| Introduction | This topic describes how to respond to a DCS failure. |

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| What will Happen | There are several failure modes possible with the DCS:   1. All process screens go blank. Caused by failure of both the UPS source (primary) and Sub 8 (secondary). 2. Multiple (mostly low hazard), but not all, process screens go blank. Caused by failure of both Server A and Server B. 3. A single process screen goes blank. Caused by failure of a single Console. 4. Multiple valves (valves only) turn purple on process screen. Caused by trip of 110 volt circuit or DCS card failure. 5. Multiple valves show purple and transmitters show NAN within a red box on process screen. Caused by failure of controller and secondary-redundant controller failure or DCS I/O card failures.   Responses to each of the above failure modes are listed on the following page. For any of these events, the DCS technician/engineer should be contacted immediately. |

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| Safety | Loss of DCS power drives all valves and motors to their failsafe positions.  If the process operates outside safety limits, the safety interlock system will shut down the process.  Wear breathing air if there is potential of being exposed to TFE vapors, for example, if you are in proximity to a TFE vent. Areas with a high potential for exposure to a TFE vent include inside the barricades (cells), the cell corridor, the blast area, and roof above the barricades.  Avoid entrance inside the barricades or the roof above the barricades while the autoclave, FPD autoclaves, or Monomer Weigh Tanks are at high-operating pressure. |

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| Environmental | When venting the monomer weigh tanks, only vent when necessary to minimize the amount of TFE vented to the atmosphere. |

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| Reference | For more information about activating the emergency vent valves, see chapter 3, this section. |

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## Responding to a DCS Failure, Continued

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| Response 1. | Follow these steps to respond to all process screens going blank: |

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| Step | Action |
| 1 | Activate the emergency shutdown pushbutton for each of the four autoclaves (1726PB, 3568PB, 2568PB, and 9070PB). |
| 2 | Contact site ECO headquarters and activate shelter in place for possible fume release. |
| 3 | Vent the autoclave by opening the emergency vent valve. Vent the autoclave for 3-5 minutes before proceeding to the next step to make sure Monomer Weigh Tank (MWT) pressure is maintained greater than autoclave pressure. |
| 4 | Using the emergency vent valves, vent any MWT that was pressurized (>90 psig) before the power outage for 30 seconds. |
| 5 | Check in the field around the monomer weigh tanks. Verify that the emergency vent valves are closed. If one of them is not closed, close the manual valve in the vent line to stop the continuous vent. |
| 6 | Monitor the pressure in the monomer weigh tanks using the field gauges. When the pressure builds up to 110 psig, vent the monomer weigh tank down by opening the emergency vent valve. Keep the pressure in the tanks below 110 psig. |
| 7 | Verify with Granular control room that automatic valves on bottom of refined monomer storage tanks are still open, and that TFE liquid has not been trapped between closed valves. |
| 8 | Continue to monitor the pressure in the monomer weigh tanks Vent as needed to prevent overpressure of a system. |
| 9 | When power comes back on, check temperatures and pressures of the TFE systems and establish brine flow as soon as possible to keep venting to a minimum.  Do not re-open automatic isolation valves until the integrity of all rupture disks is determined. |

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| Response 2. | Follow these steps to respond to multiple, but not all, process screens go blank: |

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| Step | Action |
| 1 | Log onto available screens using the operator login for area requiring action. |
| 2 | Complete any autoclave batches already in reaction, and abort all others. |
| 3 | Contact supervision to determine which autoclaves should be run on available DCS process screens. |

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## Responding to a DCS Failure, Continued

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| Response 3. | Follow these steps to respond to a single process screen going blank: |

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| Step | Action |
| 1 | Log onto available screens using the operator login for area requiring action. |
| 2 | Complete any autoclave batches already in reaction, and abort all others. |
| 3 | Contact supervision to determine which autoclaves should be run on available DCS process screens. |

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| Response 4. | Follow these steps to respond to multiple valves (valves only) turning purple on process screen: |

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| Step | Action |
| 1 | Abort any batch on the affected autoclave. |
| 2 | Check IPP 110 volt circuit panels and reset any tripped breakers. |
| 3 | If no tripped breakers are found or this does not correct the problem, contact DCS technician or engineer. |

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| Reference | For more information about activating the emergency vent valves, see chapter 3, this section. |

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#### Responding to a DCS Failure, Continued

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| Response 5. | Follow these steps to respond to multiple valves turning purple and transmitters showing NAN? Within a red box on process screen: |

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| Step | Action |
| 1 | Activate the emergency shutdown pushbutton for the affected autoclave (1726PB (#6), 3568PB (#7), 2568PB (#8), and 9070PB (#9)). |
| 2 | Contact site ECO headquarters and activate shelter in place for possible fume release. |
| 3 | Vent the autoclave by opening the emergency vent valve. Vent the autoclave for 3-5 minutes before proceeding to the next step to make sure Monomer Weigh Tank (MWT) pressure is maintained greater than autoclave pressure. |
| 4 | Using the emergency vent valves, vent any MWT that was pressurized (>110 psig) before the power outage for 30 seconds. |
| 5 | Check in the field around the monomer weigh tanks. Verify that the emergency vent valves are closed. If one of them is not closed, close the manual valve in the vent line to stop the continuous vent. |
| 6 | Monitor the pressure in the monomer weigh tanks using the field gauges. When the pressure builds up to 110 psig, vent the monomer weigh tank down by opening the emergency vent valve. Keep the pressure in the tanks below 110 psig. |
| 7 | Continue to monitor the pressure in the monomer weigh tanks. Vent as needed to prevent overpressure of a system. |
| 8 | When power comes back on, check temperatures and pressures of the TFE systems and establish brine flow as soon as possible to keep venting to a minimum.  Do not re-open automatic isolation valves until the integrity of all rupture disks is determined. |

End of topic